See discussions, stats, and author profiles for this publication at: [https://www.researchgate.net/publication/6830679](https://www.researchgate.net/publication/6830679_Simultaneous_Saccharification_and_Fermentation_of_Cassava_Bagasse_for_L--Lactic_Acid_Production_Using_Lactobacilli?enrichId=rgreq-c20c2204d514d3bd8eb628338d6d7225-XXX&enrichSource=Y292ZXJQYWdlOzY4MzA2Nzk7QVM6ODg3NzYxNjE1NzM2ODMzQDE1ODg2NzAyNzEwMzg%3D&el=1_x_2&_esc=publicationCoverPdf)

[Simultaneous Saccharification and Fermentation of Cassava](https://www.researchgate.net/publication/6830679_Simultaneous_Saccharification_and_Fermentation_of_Cassava_Bagasse_for_L--Lactic_Acid_Production_Using_Lactobacilli?enrichId=rgreq-c20c2204d514d3bd8eb628338d6d7225-XXX&enrichSource=Y292ZXJQYWdlOzY4MzA2Nzk7QVM6ODg3NzYxNjE1NzM2ODMzQDE1ODg2NzAyNzEwMzg%3D&el=1_x_3&_esc=publicationCoverPdf) Bagasse for L-(+)-Lactic Acid Production Using Lactobacilli

Article in Applied Biochemistry and Biotechnology · October 2006 DOI: 10.1385/ABAB:134:3:263 · Source: PubMed

Job: ABAB 134 Operator: KB Chapter: Nampoothiri (05-0090) Date: 5/06 Pub Date: 2006 Revision: 1st galleys **U** constant *U* constant

Copyright © 2006 by Humana Press Inc.
All includes All rights of any nature whatsoever reserved. 0273-2289/1559-0291 (Online)/06/134/0001/\$30.00

Simultaneous Saccharification and Fermentation of Cassava Bagasse for L-(+)-Lactic Acid Production Using Lactobacilli

<Au: Pls. proofread carefully.

ROJAN P. JOHN, K. MADHAVAN NAMPOOTHIRI,* AND ASHOK PANDEY

Biotechnology Division, Regional Research Laboratory (CSIR) Trivandrum–695 019 Kerala, India, E-mail: madhavan85@hotmail.com

> **Received October 27, 2005; Revised February 3, 2006; Accepted February 20, 2006**

Abstract

Biotechnology Division,

Research Laboratory (CSIR) Trivandrum-695 019 Kerala

E-mail: madhavan85@hotmail.com

Received October 27, 2005; Revised February 3, 2006;

Accepted February 20, 2006

the corrected February 20, 20 Accepted February 20, 2006
 Proof Conception Accepted February 20, 2006
 Proof Conception of cassava (Manihot esculenta) bagasse
 Probabilizes
 Probabilizes
 Probabilizes
 Probabilizes
 Probabilizes
 Probabi Saccharification and fermentation of cassava (*Manihot esculenta*) bagasse was carried out in a single step for the production of $L^{(+)}$ -lactic acid by *Lactobacillus casei* and *Lactobacillus delbrueckii*. Using 15.5% w/v of cassava bagasse as the raw material, a maximum starch to lactic acid conversion of 96% was obtained with *L. casei* with a productivity rate of 1.40 mg/mL·h and maximum yield of 83.8 mg/mL. It was 94% with *L. delbrueckii* with a productivity rate of 1.36 mg/mL·h and maximum yield of 81.9 mg/mL. Supplementation of bagasse with 0.01% w/v MnCl, showed positive influence on the lactic acid production by *L. casei.*

Index Entries: Cassava bagasse; L-(+)-lactic acid; *lactobacilli*; simultaneous saccharification; fermentation.

Introduction

Lactic acid is widely used in food and nonfood industries, such as cosmetics, pharmaceuticals, textile, leather, and other chemical industries, because of the versatile applications of it and its salts. Currently the demand of lactic acid is increased as a result of the environmentally friendly nature of its polymer, polylactic acid *(1–5)*. Lactic acid is commercially produced by chemical synthesis and fermentation. By microbial fermentation, we can

*Author to whom all correspondence and reprint requests should be addressed.

Applied Biochemistry and Biotechnology and $\frac{1}{2}$ a

1

py

2 John, Nampoothiri, and Pandey

produce the desired isomer, whereas chemical synthesis yields only the racemic mixture *(3,5)*. Lactic acid produced from cheaper starchy substrate can replace the refined sugars *(6)*. Conventional lactic acid production from starchy materials, such as corn, barley, or rice, requires gelatinization, liquefaction, and saccharification before fermentation by lactic acid bacteria. But these processes are not economical because of the high-energy needs for the liquefaction *(7)* and because the production of lactic acid will be inhibited when the sugar concentration is high in the medium. The microbial fermentation coupled with enzymatic hydrolysis of starch has many benefits. This process can decrease the inhibition as a result of the high glucose accumulation and also reduces the reactor volume and the cost of the process *(2)*. Some of the researchers tested simultaneous saccharification and lactic acid production from cellulose *(8,9)*. This can be done using lactic acid producing fungi like *Rhizopus(10).* But the conversion efficiency of the fungus is less than that of bacteria *(11).* Linko and Javanainen *(7)* had reported the simultaneous saccharification and fermentation of barley starch for lactic acid production using *Lactobacillus. casei* with the help of starch hydrolyzing enzymes.

for lactic acid production using *Lactobacillus*. casei with
hydrolyzing enzymes.
assava (*Manihot esculenta*) ranks the world's sixth most
op and is the basic food for more than seven hundred mill
rral countries (12). The urge family that is extensively cultivated as an annua
archy tuberous root. Industrial application of cassave
quantity of solid bagasse and it is generally discarded
is a landfill without any treatment. Its disposal is a s Cassava (*Manihot esculenta*) ranks the world's sixth most important food crop and is the basic food for more than seven hundred million people in several countries *(12).* The cassava, or manioc, is a woody perennial shrub of the spurge family that is extensively cultivated as an annual crop for its edible starchy tuberous root. Industrial application of cassava generates a large quantity of solid bagasse and it is generally discarded in the environment as a landfill without any treatment. Its disposal is a serious concern to the environment *(12,13).* Cassava bagasse is a fibrous residue, which contains about 52% starch on a dry weight basis *(14).* In this work, we tried a single-step conversion of the cassava bagasse for the production of L-(+)-lactic acid using two *lactobacilli* namely *Lactobacillus delbrueckii* and *L. casei* and compared their nutritional and other physico-chemical requirements in the production.

Materials and Methods

Microorganism

Homofermentative *L. delbrueckii* NCIM 2025 producing L-lactic acid was procured from National Collection of Industrial Microorganism, National Chemical Laboratory, Pune, India and *L. casei* NCIMB 3254 was obtained from National Collection of Industrial and Marine Bacteria Ltd., Aberdeen, Scotland. Strains were maintained as stab culture at 4°C on MRS agar and when required the strains were revived by propagation at 37°C for 18 h in MRS broth.

Enzymes

For the enzymatic hydrolysis of cassava bagasse, commercially available (Rashesh and Co., Mumbai, India) α -amylase (Termamyl, 5000 IU/mL) and glucoamylase (AMG, 2000 IU/mL) procured were used.

Applied Biochemistry and Biotechnology Vol. 134, 2006

Job: ABAB 134 Operator: KB Chapter: Nampoothiri (05-0090) Date: 5/06
Pub Date: 2006 Revision: 1 **U** constant *U* constant

Simultaneous Saccharification and Fermentation of Cassava Bagasse 3

Saccharification and Fermentation

Unless it is otherwise emphasized, the production medium was made by supplementing the raw cassava bagasse $(15.5\% \text{ w/v})$ in 100 mL distilled water with yeast extract $(0.5\% \text{ w/v})$ and ammonium chloride $(0.5\% \text{ w/v})$. Tween-40 (0.4% v/v) was added as surfactant and $CaCO₃(4\% \text{ w/v})$ was added for buffering (to keep the medium pH between 5.5–6.5). Fermentation medium was autoclaved at 121°C (15 lb) for 15 min. Subsequently, the sterile medium was inoculated with 2.5 mL preparatory culture (18 h, CFU/mL 109) of *L. delbrueckii* and *L. casei*. Sufficient amounts of both starch-hydrolyzing enzymes were also added to the inoculum. After thorough mixing, the flasks were incubated in static condition at 37°C in an environmental chamber (Sanyo, Japan) for 3 d.

Optimization of Parameters for Lactic Acid Production

box and pays to the main state of sacharacted on. In order to optimize it, different amounts of bagasse (tried for each organism. Similarly effective conversion dar consumption rate and it indirectly depends on the biddiff If volumes (1, 1.3, 2, 2.3, 3, 3, 3, 3, 3) and 4% [V/V]) of 18 if ord;
d; each culture was diluted to approx 10^9 cells per 1 m
cubation time for complete utilization of sugar and al
accumulation of lactic acid, the The amount of reducing sugar available will depend upon the amount of initial cassava bagasse concentration subjected for saccharification and fermentation. In order to optimize it, different amounts of bagasse (2–17%, w/v) were tried for each organism. Similarly effective conversion depends on the sugar consumption rate and it indirectly depends on the biomass. Because the amount of inoculum is critical in-deciding the biomass formation different volumes (1, 1.5, 2, 2.5, 3, 3, 5, and 4% [v/v]) of 18 h old cultures were tested; each culture was diluted to approx 109 cells per 1 mL. To optimize the incubation time for complete utilization of sugar and also for the maximum accumulation of lactic acid, the inoculated flasks were incubated for different time intervals (12, 24, 36, 48, 60, 72, and 84 h). Samples were withdrawn at regular intervals and the level of sugar and lactic acid were determined. Apart from the carbon source, the organism is in need of a readily available nitrogen source. Ammonium chloride at different levels $(0.25, 0.5, 1, 1.5, 2, \text{and } 2.5\%$ [w/v]) was supplemented to optimize its level. Because lactobacilli are known as fastidious organisms, yeast extract was shown to have good influence on their growth as it contains many vitamins, amino acids, and other nutrients. Thus different concentrations of yeast extract (0.25, 0.5, 1, 1.5, 2, 2.5, and 3% [w/v]) were tested to achieve maximum growth and product yield. To study the influence of temperature on productivity, fermentation experiments were carried out at different temperatures (30, 37, 42, and 51°C). Other parameters studied include the effect of manganese chloride $(0, 0.01, 0.025,$ and 0.05% [w/v]) on lactic acid production and the amount of CaCO_{3} requirement (1, 2.5, 4, 5.5, and 7% [w/v]) for effective buffering of the production medium. For comparison, a control flask without CaCO $_{_3}$ was included. In order to see the effect of MnCl $_{_{2^{\prime}}}$ the ammonium chloride concentration in all the cases, including the control, was reduced from 0.5 to 0.4% (w/v) to avoid excess chloride.

Analysis

Applied Biochemistry and Biotechnology Vol. 134, 2006 Samples were withdrawn at desired intervals, treated, and diluted with $1 M \rm H_2SO_4$ to release lactic acid from calcium lactate. Total lactic acid

py

4 John, Nampoothiri, and Pandey

(mg/mL fermentation medium) was estimated according to the colorimetric method of Barker and Summerson *(15)*. The amount of reducing sugar was determined by the dinitrosalicylic acid method *(16).* Starch was estimated photometrically as described by Nampoothiri et al. *(17)* using an aqueous iodine solution as a reagent; coloration of samples was measured on a UV spectrophotometer (Shimadzu, Japan) at 620 nm. All the experiments were performed in triplicate. The estimation of biomass was interfered by cassava bagasse as the bacterial cells are entrapped and mixed with the bagasse in the fermentation medium. Therefore, the biomass estimation was omitted from the current study and generally the conversion of medium components to biomass was negligible in the case of anaerobic lactic acid fermentation by *lactobacilli*.

Results and Discussion

gelatinized starch is much different from the fermential
and it can affect the initial growth of the bacteria as w
in terms of lactic acid yield. For example, in a separate
ysis of starch, the optimum pH and temperature f provided in simultaneous application of the substrate conception of the series of the series wever, the strategy we adopted in simultaneous saccel mentation experiments was different. The enzymes r with the lactobacilli an The optimum temperature and pH for liquefaction and saccharification of gelatinized starch is much different from the fermentation conditions and it can affect the initial growth of the bacteria as well as later growth in terms of lactic acid yield. For example, in a separate enzymatic hydrolysis of starch, the optimum pH and temperature for α-amylase reaction was 5 and 90 \degree C and for glucoamylase it was 4 and 60 \degree C respectively. Under these optimum circumstances a ready release of reducing sugar will take place. However, the strategy we adopted in simultaneous saccharification and fermentation experiments was different. The enzymes were added together with the lactobacilli and the medium pH was 6.0–6.5 and temperature 37°C. Under these conditions the enzymes may not show their optimum level of activity, but a partial level activity is expected. This will help the controlled release of sugars and is very crucial for the fermentation in such a way that even if we use a highly starchy material, feedback inhibition resulting from a higher reducing sugar level will not take place. External supplementation of the enzyme was necessary because both of the strains do not possess any amylolytic activity. Also, under these conditions, the bacteria can grow well to consume the available sugars and to make lactic acid. Interestingly we found that in all the substrate concentrations used for the fermentation, simultaneous saccharification and fermentation had much more productivity than the simple saccharification and fermentation even if the temperature and pH were very far from the optimum (data not shown). Linko and Javanainen (7) reported 66% of conversion from starch to sugar during the saccharification at 37°C on barley starch after 24 h. When the temperature rose to 60°C there was only a slight increase, after 24 h the yield was only 69%. In our experiments we performed saccharification as well as the fermentation at pH 6.5 and 37°C.

The initial concentration of cassava bagasse was optimized as 15.5% (w/v) (Fig. 1) as it had the high conversion rate and high production. Further increase of the bagasse amount makes the medium a slurry type, which will readily solidify and negatively influence the mixing of enzymes and

Fig. 1

Applied Biochemistry and Biotechnology Vol. 134, 2006

Simultaneous Saccharification and Fermentation of Cassava Bagasse 5

Fig. 1. Optimization of cassava bagasse concentration for simultaneous saccharification and fermentation; *L. delbrueckii* (\blacklozenge) , *L. casei* (\square).

Cassava bagasse concentration for simultaneous sacrimization of cassava bagasse concentration for simultaneous sacrimentation; *L. delbrueckii* (\bullet), *L. casei* (\Box).

However, we found an initial level of 15. Five per From the process. When we made the hydrolysate by enzythe a shake-flask fermentation is really the best level of the process. When we made the hydrolysate by enz om cassava bagasse and used the hydrolysate for found more t inoculum. However, we found an initial level of 15 . Five percent (w/v) of starchy material in a shake-flask fermentation is really the best level of the raw material to start the process. When we made the hydrolysate by enzymatic treatment from cassava bagasse and used the hydrolysate for fermentation, it was found more than 7.5% (w/v) of starch cannot be used. We observed a kind of feedback inhibition as a result of higher glucose level in the hydrolysate (data not shown). Because of the controlled release of sugars and its utilization in simultaneous saccharification and fermentation, a higher level of initial raw material can be used.

Hujanen and Linko *(18)* have reported that 90% yield (121 g/L lactic acid from 130 g/L glucose supplemented with 20 g/L yeast extract by 15% inoculum of *L. casei.* The low lactic acid production rate was as a result of the high glucose concentration and production temperature. In this present study, 2% (v/v) inoculum is needed for the *L. casei* NCIMB 3254. However, 2.5% (v/v) inoculum was the optimum for *L. delbrueckii* NCIM 2025 (Fig. 2).

Lactic acid bacteria generally have complex nutrient requirements for the growth and fermentation *(5,19)*. In case of *L. delbrueckii* NCIM 2025 and *L. casei* NCIMB 3254, optimum yeast extract concentration was 0.5% (w/v) for the maximum conversion (Fig. 3). Lower concentrations had a negative effect on the productivity. This observation is in good agreement with the report on lactic acid production from date juice using *L. casei(20)*. There was no influence of yeast extract in higher concentrations.

Similarly, as shown in Fig. 3, an optimum of 0.5% (w/v) of NH₄Cl was supplemented in the production medium along with 0.5% (w/v) of yeast extract, which serves as a readily available nitrogen source for the organism.

Applied Biochemistry and Biotechnology Vol. 134, 2006

Uncorrected Proof Copy

Fig. 2

Fig. 3

Revision: 1st galleys **py**

6 John, Nampoothiri, and Pandey

Fig. 2. Optimization of inoculum size; *L. delbrueckii* (□), *L. casei* (■) for the lactic acid production.

Fig. 3. Optimization of yeast extract concentration; *L. delbrueckii* (\triangle), *L. casei* (\diamond) and ammonium chloride concentration; *L. delbrueckii (* \Box), *L. casei (* \Box *) for the production of* lactic acid.

A time course study showed that for both *L. delbrueckii* and for *L. casei* the lactate production reached a plateau after 60 h. Further increase in fermentation time did not enhance the yield. As it is shown in Fig. 4, the

Uncorrected Proof Copy

Fig. 4

Simultaneous Saccharification and Fermentation of Cassava Bagasse 7

maximum production of lactic acid using *L. delbrueckii* was 79.5 mg/mL and it was 81.5 mg/mL for *L. casei.*

INCOVERTY IN THE INTERET SET AND PROPERTIES ASSESSMENT CONSTRAINS A SERVING DETERMIND Production of lactic acid using *L***, delbrueckii was 79.5 n

B1.5 mg/mL for** *L. casei.***

acid bacteria have a wide range of temperatur** tion of lactic acid using *L*, delbrueckii was 79.5 mg/n

g/mL for *L. casei.*

neteria have a wide range of temperature optimum f

ion. Linko and Javanainen (7) showed that with *L. ca*

rsion of 87-98% was occurred at 3 Lactic acid bacteria have a wide range of temperature optimum for lactic acid production. Linko and Javanainen *(7)* showed that with *L. casei* an optimum conversion of $87-\frac{98}{6}$ was occurred at 37° C and it was 77–82% at 41°C. Anuradha et al. *(2)*, conducted experiment with *L. delbrueckii* at a temperature of $40-50^{\circ}$ and obtained a 70% conversion of starch. In this study, maximum production was noted when both the organisms were incubated at 37°C (80.6 mg/mL in the case of *L. casei* and 74.4 mg/mL for *L. delbrueckii*). At all temperatures *L. casei* had the better yield than *L. delbrueckii*, except at 44°C (Fig. 5).

Fig. 6

Interestingly, as shown in the Fig. 6, we observed that the presence MnCl₂ in lower concentration level (0.01% [w/v]) enhanced the lactic acid production in the case of *L. casei.* However, in higher concentrations, it had an inhibitory effect and the production is less than that of the control one. In the case of *L. delbrueckii*, the MnCl₂ did not show any positive effect.
-In comparison to our observation there are reports of enhanced lactic acid production in presence of MnCl₂ with *L. casei* (21).

Calcium carbonate plays a crucial role in the lactic acid fermentation as it buffers the medium. During the production of lactic acid, it is converted to calcium lactate and maintains the pH. The presence of 2.5–4% (w/v) of calcium carbonate in the production medium was found to be good for lactic acid production in both the cases. In the control, the accumulation of lactic acid is inhibited because of the lowering of pH, which adversely affected the bacterial growth. After 60-h fermentation under regulated

Uncorrected Proof Copy

py

8 John, Nampoothiri, and Pandey

 $\operatorname{Fig. 6.}$ Optimization of MnCl₂; *L. delbrueckii (*□), *L. casei (*■).

pH conditions, *L. casei* produced 83.8 mg/mL of lactic acid with a conversion (sugar to lactic acid) of 96.3% and for *L. delbrueckii* it was 81.9 mg/mL with a conversion of 94.1%. The rate of productivity was calculated accordingly. Data are shown in the Fig. 7.

Woiciechowski et al. *(13)* studied the hydrolysis of cassava bagasse starch by acid and enzymatic hydrolysis and reported that both the methods were quite efficient depending on the percentage of hydrolysis, time, and cost of the chemicals and energy consumption. According to them, the

Uncorrected Proof Copy

Job: ABAB 134 Operator: KB Chapter: Nampoothiri (05-0090) Date: 5/06 Pub Date: 2006 Revision: 1st galleys **U** constant *U* constant

Simultaneous Saccharification and Fermentation of Cassava Bagasse 9

Fig. 7. Optimization of CaCO₃ concentration; *L. delbrueckii* (□), *L. casei* (◆).

Optimization of CaCO₃ concentration; *L. delbrueckii* (□), *L. casei* (

hydrolysis of 150 kg cassava bagasse itself is required a

advantage of simultaneous saccharification is that it avo

ydrolysis step and reduces t enzymatic hydrolysis of 150 kg cassava bagasse itself is required around \$2471. The advantage of simultaneous saccharification is that it avoids the separate hydrolysis step and reduces the cost of energy consumption for the liquefaction and saccharification Hence it is cost effective and time saving process for the lactic acid production.

Conclusion

Is step and redaces the cost of energy consumption is
not saccharification Hence it is cost effective and tir
the lactic acid production.
we and eco-friendly method was adopted with the val
assaya bagasse, which contains n A cost-effective and eco-friendly method was adopted with the valuable addition of cassava bagasse, which contains nearly 52% entrapped starch. A single step conversion of cassava starch present in the bagasse to L-lactic acid is demonstrated using two lactobacilli. The tedious preparation of separate starch hydrolysate either by the enzymatic or chemical methods is avoided with the simultaneous saccharification and fermentation process. Also, a comparatively large amount of initial raw material can be used because there is a controlled release of sugar and its immediate use. Hence, the uncompetitive inhibition by the substrate generally observed while using starch hydrolysate because of high the concentration of sugar is avoided.

Acknowledgments

One of the authors (RPJ) is deeply indebted to the Council of Scientific and Industrial Research (CSIR) for the award of Junior Research Fellowship for doctoral studies. The authors would like to thank the CSIR Task force network program on green technology (CMM 0006) for providing financial support.

Applied Biochemistry and Biotechnology Vol. 134, 2006

py

10 John, Nampoothiri, and Pandey

References

- *1.* Dimerci, A., Pometto III, A. L., and Johnson, K. E. (1993) *Appl. Environ. Microbiol.* **59,** 203–207.
- *2.* Anuradha R., Suresh A. K., and Venkatesh K. V. (1999) *Proc. Biochem*. **35,** 367–375.
- *3.* Pandey, A., Soccol C. R., Jose A., Rodriguez-leon, and Nigam P. (2001), in *Solid State Fermentation in Biotechnology: Fundamentals and Applications*, Asiatech Publishers, New Delhi, India, pp. 81–131.
- *4.* Yun, J., Wee, Y., and Ryu, H. (2003) *Enzyme Microb. Technol*. **33,** 416–423.
- *5.* Yun, J., Wee, Y., Kim, J., and Ryu, H. (2004) *Biotechnol. Lett*. **18,** 1613–1616.
- *6.* Naveena, B. J., Vishnu, C., Altaf, Md., and Reddy, G. (2003) *J. Sci. Ind. Res*. **62,** 453–456.
- *7.* Linko, Y. Y. and Javanainen P. (1996) *Enzyme Microb. Technol*. **19,** 118–123.
- *8.* Abe, S. and Takagi, M. (1991) *Biotechnol. Bioeng*. **37,** 93–96.
- *9.* Venkatesh, K. V. (1997) *Biores. Technol*. **62,** 91–98
- *10.* Yu, R. U. and Hang, Y. D. (1989) *Biotechnol. Lett*. **11,** 597–600.
- *11.* Naveena B. J. (2004), Ph D Thesis, Osmania University, Hyderabad, India.
- *12.* Pandey, A., Soccol, C. R., Nigam, P., Soccol, V. T., Vandenbergh, L. P. S., and Mohan, R. (2000) *Biores. Technol*. **74,** 81–87.
- *13.* Woiciechowski, A. L., Nistsche, S., Pandey, A. and Soccol, C. R. (2002) *Braz. Archives Biol. Technol*. **45,** 393–400
- *14.* Carta, F. S., Soccol, C. R., Ramos, L. P., and Fontana, J. D. (1999) *Biores. Technol*. **68,** 23–28.
- *15.* Barker, S. B. and Summerson, W. H. (1941) *J. Biol. Chem*. **138,** 535–554.
- *16.* Miller, G. L. (1959) *Anal. Chem*. **31,** 426–429.
- *I. Fermini. 43, 335*–333.

Irta, F.S., Soccol, C.R., Ramos, L.P., and Fontana, J.D. (1999) Biores, Tech

rker, S. B. and Summerson, W. H. (1941) *J. Biol. Chem.* **138**, 535–554.

iller, G. L. (1959) *Anal. Chem.* **31**, 42 *17.* Nampoothiri, K. M., Singhania, R. R., Sabarinath, C., and Pandey, A. (2003) *Proc. Biochem*. **38,** 1513–1519.
- *18.* Hujanen, M. and Linko, Y. Y. (1994) *Biotechnol. Tech*. **8,** 325–333.
- *19.* Hofvendahl, K. and Hahn-hagerdal, B. (2000) *Enzyme. Microb. Technol*. **26,** 87–107.
- and Linko, F. F. (1994) Biotechnol. 1ech. 6, 3z5-353.
 R. and Hahn-hagerdal, B. (2000) Enzyme. Microb. Technol. 26, 8

Nancib, N., Meziane-cherif, D., Boudenbir, A., Fick, M., and Bout
 R. Technol. 96, 63-67

Tinsdill, *20.* Nancib, A., Nancib, N., Meziane-cherif, D., Boudenbir, A., Fick, M., and Boudrant, J. (2005) *Biores. Technol*. **96,** 63–67.
- *21.* Frobisher, Hinsdill, Crabtree, and Goodheart. (1974), in *Fundamentals of Microbiology*, W B Saunders Company, Philadelphia, PA, pp. 783-784.

<AU: Pls. provide the name of the editor for the book in reference 21.

<AU: Pls. provide the name of the editor for the book in reference 3.